

Effects of system parameters and inorganic salts on the photodecolourisation of textile dye Reactive Blue 19 by UV/H₂O₂ process

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ABSTRACT

The photodecolourisation of textile dye Reactive Blue 19 (RB 19), an anionic anthraquinone dye of the reactive class, was investigated using UV radiation in the presence of H₂O₂ in a batch photo-reactor with low-pressure mercury lamps. The effects of the system parameters: initial pH, initial dye concentration, concentration of peroxide and radiation intensity, as well as the presence of salts, (NaCl, Na₂SO₄, NaNO₃, NaH₂PO₄) on dye decolourisation was examined. Increasing the initial pH resulted in an increase in decolourisation efficiency. Results showed that with an increase of dye concentration from 10 to 100 mg·ℓ⁻¹, the efficiency of the process decreases. The highest decolourisation rates were noted at H₂O₂ concentrations of approximately 30 mmol·ℓ⁻¹. The increase of radiation intensity from 730 to 1 950 μW·cm⁻², linearly increases decolourisation efficiency. The inorganic ions investigated have inhibiting effects on RB 19 decolourisation by the UV/H₂O₂ process with inhibition intensities in the following order: H₂PO₄⁻ > NO₃⁻ > SO₄²⁻ > Cl⁻. This study has shown that the UV/H₂O₂ process is a promising technology for degradation of RB 19 in water and wastewater.

Keywords: UV/H₂O₂ process, Reactive Blue 19, decolourisation, inorganic salts

INTRODUCTION

In the textile industry, the dyeing process produces large quantities of wastewater with intense colouration that has to be eliminated before release into the environment. Wastewaters from the textile industries contain different types of synthetic dyes, which are mostly toxic, mutagenic and carcinogenic (Zollinger, 2003; Song et al., 2008). There are many structural varieties of dyes, such as azo, anthraquinone, phthalocyanine, direct, reactive, dispersive, acid, basic, neutral and metal complexed. The three most commonly used groups of dyes are azo, anthraquinone and phthalocyanine (Ghodbane et al., 2010). There are a number of reasons why reactive dyes are the most often used in the dyeing process, e.g., good stability during washing, and relatively simple dyeing procedures (Kurbus et al., 2002; Muruganandham et al., 2004). These dyes are the most common in use today especially for dyeing of wool and cellulosic fibres such as cotton. Reactive dyes, which have good water solubility and are easily hydrolysed into insoluble forms, are extensively used in dyeing processes, and about 20–40% of these dyes remain in the effluent (Armagan et al., 2003). Thus, an effective and economical technique for removing reactive dyes from textile wastewater is needed.

In past decades, some techniques such as adsorption, membrane separation, coagulation, chemical oxidation, and electrochemical degradation have been investigated to treat

dyeing wastewater. However, low removal efficiency or high cost in operation often limits their application (Wang et al., 2008). In recent years, advanced oxidation processes (AOPs) have been developed to treat the contaminants of natural water and industrial effluents. Earlier studies have shown that anthraquinone dyes can be removed by ozone (Kunc et al., 2002; Chen et al., 2009; Fanchiang et al., 2009), the combination of ozone and ultrasound, or electrochemical degradation in natural waters and effluents from the textile industry (He et al., 2008; Kim et al., 2002; Rajkumar et al., 2007). TiO₂ and TiO₂-based catalysts were used for the photodegradation of anthraquinone dyes (Saqib et al., 2002; Lizama et al., 2002). Colonna et al. (1999) reported that homogenous advanced oxidation processes employing hydrogen peroxide with UV light lead to complete decolourisation and mineralisation of sulphonated azo and anthraquinone dyes. This process is based on the generation of hydroxyl radicals (•OH), and a strong oxidising agent (E⁰ = 2.8 V), which degrade a broad range of organic pollutants quickly and non-selectively (Muruganandham et al., 2004; Aleboyeh et al., 2005; Daneshvar et al., 2005). Reaction of hydroxyl radicals generated in the presence of an organic substrate may occur via one of three general pathways: (i) hydrogen abstraction; (ii) electrophilic addition and (iii) electron transfer (Daneshvar et al., 2005). The method is inexpensive and non-toxic for treatment of water (Bilgi et al., 2005).

For practical application of the UV/H₂O₂ process for treatment of dye-contaminated wastewater, it is important to determine the optimal experimental conditions. In this paper, the effects of initial pH, initial dye concentration, initial concentration of H₂O₂ and the presence of inorganic salts on decolourisation of reactive dye C.I. Reactive Blue 19 (RB 19) by UV radiation in the presence of hydrogen peroxide were examined.

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TABLE 1 General characteristics of RB 19					
Molecular formula	Molecular mass (g·mol ⁻¹)	λ_{\max} (nm)	CAS number	C.I. number	IC ₅₀ (mg·l ⁻¹)
C ₂₂ H ₁₆ N ₂ Na ₂ O ₁₁ S ₃	626.55	592	2580-78-1	61200	55

EXPERIMENTAL

Reagents

The anthraquinone reactive dye C.I. Reactive Blue 19 (RB 19) (molecular weight 626) was obtained from Sigma-Aldrich (USA) and used without any purification. Table 1 summarises the general characteristics of RB 19. The H₂O₂ solution (30%) and other used reagents (NaCl, Na₂SO₄, NaNO₃, and NaH₂PO₄) were of analytical grade and purchased from Merck (Germany).

Procedures

A stock solution of RB 19 was made by dissolving 1.00 g dye in 1 000 ml deionised water. Working solutions were freshly prepared, before irradiation, by diluting the stock to the desired concentration with deionised water. The pH of the solutions was adjusted by addition of NaOH or HCl (0.1/0.01 mol·l⁻¹) measured with a pH-meter (SensIon5, HACH, USA). All photochemical experiments were carried out in a batch photo-reactor constructed in our laboratory facility and described in Mitrovic et al. (2012). During irradiation, the solution was magnetically stirred (Are, Velp Scientifica, Italy) at a constant rate and temperature was maintained at 25 ± 0.5°C. At required time intervals, 4 ml of samples were withdrawn and absorbance at 592 nm was measured using a UV/vis spectrophotometer Cintra 1010 (GBC, Australia) to determine the degree of decolourisation of the solution. The removal (%) of RB 19 dye was calculated as:

$$\text{Removal (\%)} = \left[1 - \frac{c_t}{c_0} \right] \times 100 \quad (1)$$

where:

c_0 and c_t are the concentration values of the dye solution before and after UV irradiation, respectively.

The total organic carbon (TOC) was also determined in order to evaluate the mineralisation rate, as an important indicator of treatment effectiveness. The TOC content was determined by a Shimadzu TOC-5000A analyser.

All experiments were carried out with 3 replicates. Average values ± SD (error bars) are presented in all graphs. All statistical tests were performed by OriginPro 8 (OriginLab, USA) using a one-way ANOVA parametric method. The strength of the relationships, measured by the correlation coefficient (R^2), as well as the significance of the relationships, expressed in probability levels (p -values) was tested. Obtained correlation coefficients were statistically significant at a significance level of 95% for all tests performed.

RESULTS AND DISCUSSION

Reactive dye C.I. Reactive Blue 19 (RB 19) was chosen as a representative of reactive dyes from the class of anthraquinones. It is characterised by high chemical stability and its

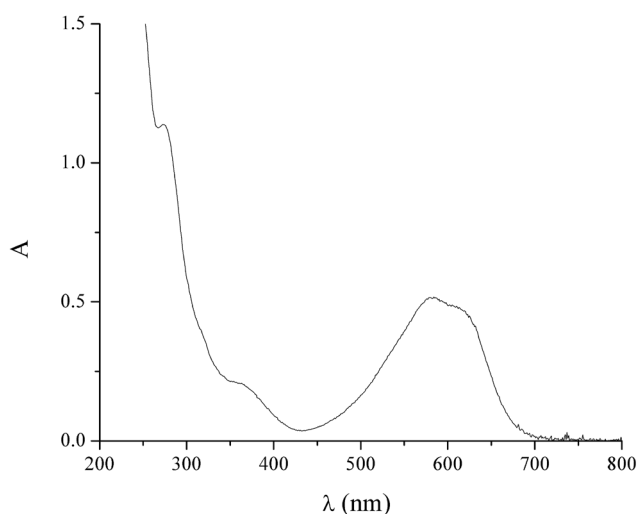


Figure 1
Absorption spectra of textile dye Reactive Blue 19

resistance to numerous physical and chemical influences present in the environment, where RB 19 can be found as a contaminant (Chang et al., 1986). The UV/vis absorption spectrum of RB 19 is presented in Fig. 1. Two absorbance peaks were observed during the scanning of the dye at pH 7.0. The visible peak at 592 nm is due to the blue colour of the dye chromophore. The peak observed in the UV region from 200 to 300 nm is due to the anthraquinone structure of the dye.

A basic photodecolourisation experiment was conducted for a time period of 20 min (initial dye concentration was 50.0 mg·l⁻¹, an initial H₂O₂ concentration of 25.0 mmol·l⁻¹, and UV radiation intensity of 1 950 μW·cm⁻²). Decolourisation was monitored by measuring of absorbance at 592 nm. The experimental results showed that the process is quite rapid and that most of the decolourisation was observed in the first 10 min of UV irradiation (85.7±4.1%), while in a period of 15 min complete decolourisation of samples was observed (Fig. 2). On the other hand, monitoring the absorbance peak at 230 nm during treatment suggested that degradation of the aromatic part of the dye molecule was a relatively slower process and incomplete in the investigated period of 20 min. R^2 values were 0.983 and 0.990 for the curves at 230 and 592 nm, respectively.

Figure 3 presents the difference between change of solution colour and TOC during the degradation of 50.0 mg·l⁻¹ RB 19. The complete removal of colour was achieved within a short period of time (15 min). In the same time, TOC removal was 15.8±0.8%, while almost complete removal of 93.5±4.7% was achieved after 240 min. It is well known that the removal of colour is due to cleavage of chromophore bonds in the dye molecule, which is a faster process than the complete oxidative degradation of molecules of dye to low molecular mass compounds (Mitrovic et al., 2012; Guimaraes et al., 2012).

A combination of UV light and H₂O₂ is required for production of •OH radicals by photolysis of the H₂O₂. The

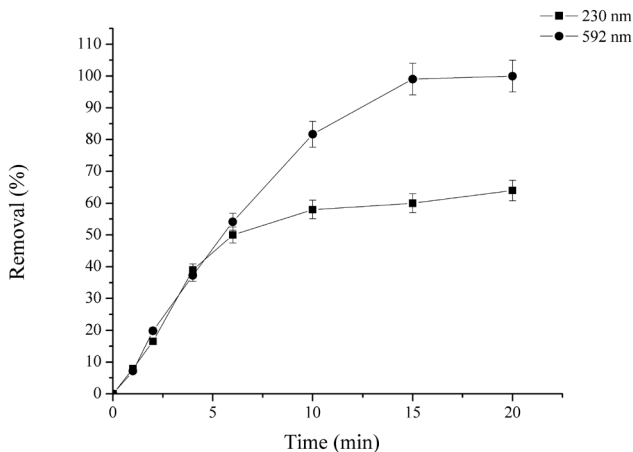


Figure 2
Removal of dye RB 19 by UV/H₂O₂ process. [RB19]₀ = 50 mg·L⁻¹, [H₂O₂]₀ = 25 mmol·L⁻¹, initial pH 7, UV radiation intensity was 1 950 μW·cm⁻², temperature was 25.0 ± 0.5°C.

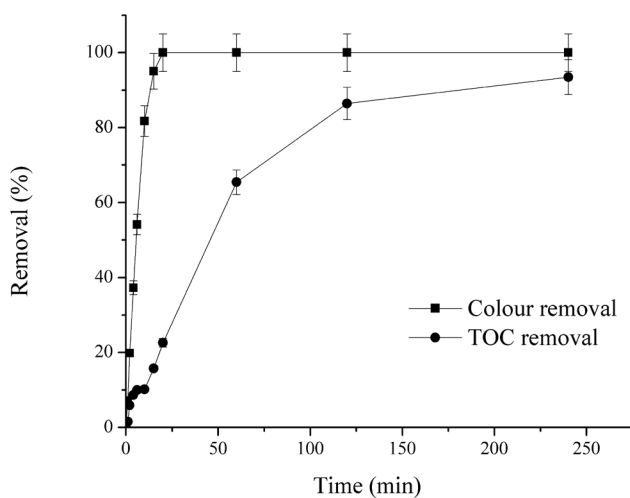
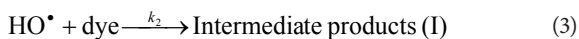


Figure 3
Change of colour and TOC during UV/H₂O₂ treatment of RB 19

hydroxyl radical is a non-selective and very powerful oxidising agent and can initiate the decolourisation reactions by reacting with the dye molecules (Zollinger, 2003; Muruganandham et al., 2004; He et al., 2008; Aleboye et al., 2005; Daneshvar et al., 2005; Aleboye et al., 2003; Daneshvar et al., 2003).



According to the results of other studies (El-Dein et al., 2003; Dong et al., 2007; Mitrovic et al., 2012), the photodecolourisation is a pseudo-first order reaction with respect to the dye concentration. The kinetic pathway of decolourisation could be expressed as follows:

$$-\frac{dc_t}{dt} = k_{app} c_t \quad (5)$$

where:

k_{app} (min⁻¹) is the apparent pseudo-first rate constant, c_t is the concentration of dye after irradiation time t .

pH	k_{app} (min ⁻¹)	R^2
2	0.0777	0.9804
3	0.0797	0.9879
4	0.0816	0.9869
5	0.0977	0.9832
7	0.1113	0.9898
9	0.1305	0.9904
10	0.1684	0.9949
11	0.1816	0.9967

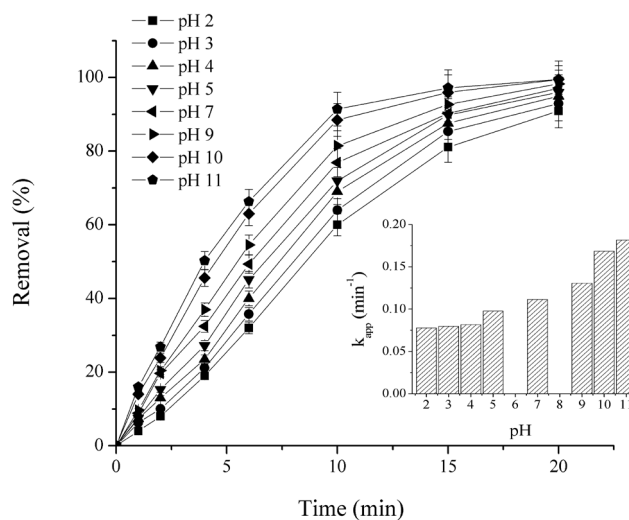


Figure 4
Effect of initial pH on removal of RB 19. [RB19]₀ = 50 mg·L⁻¹, [H₂O₂]₀ = 25 mmol·L⁻¹, UV radiation intensity was 1 950 μW·cm⁻², temperature was 25.0 ± 0.5°C. Inset shows the relation between pseudo-first order rate constants and initial pH.

This equation, after integration with the initial condition (c_0 for $t = 0$), leads to:

$$\ln(c_t/c_0) = -k_{app} t \quad (6)$$

where:

k_{app} (min⁻¹) is the apparent pseudo-first rate constant, c_t is the concentration of dye after irradiation time t , c_0 is the dye concentration at $t = 0$.

The apparent reaction rate constants (k_{app}) for decolourisation of RB 19 were calculated from semi-logarithmic graphs of $\ln(c_t/c_0)$ versus time, using the linear regression method. The values were also calculated for R^2 (0.989 for colour removal and 0.987 for TOC removal).

Effect of initial pH

The effect of pH on the rate of decolourisation of textile dye RB 19 with UV/H₂O₂ process was studied at pH values of 2, 3, 4, 5, 7, 9, 10 and 11. For an initial dye concentration of 50.0 mg·L⁻¹ and initial H₂O₂ concentration of 25 mmol·L⁻¹, the initial decolourisation rate at different pH values is shown in Fig. 4.

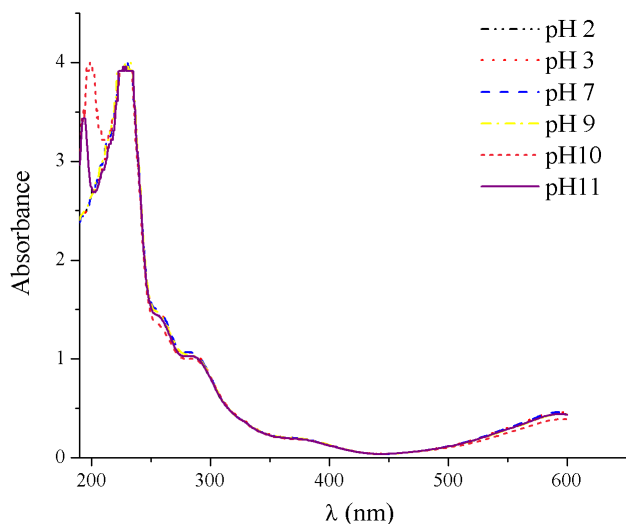
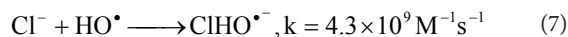


Figure 5

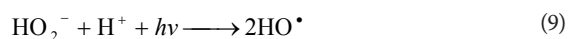
Absorption spectra of textile dye Reactive Blue 19 at different pH values. $[RB19]_0 = 50 \text{ mg}\cdot\text{L}^{-1}$.

Decolourisation efficiency increased with increasing pH from 2 to 11. The values of the apparent pseudo-first rate constant, k_{app} , and correlation coefficient (R^2) are presented in Table 2. In all experiments, the values of R^2 were higher than 0.98.

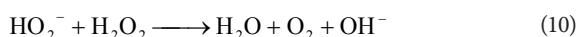
For an acidic pH, with acidification of the solution by HCl (dye solution with initial pH 2, 3, 4 and 5), the amounts of conjugated base Cl^- ions increase. The anion Cl^- can react with $\bullet\text{OH}$ leading to the formation of inorganic radical ions $\text{ClOH}\bullet^-$ (Reaction (7)) (Aleboye et al., 2005; Jaysona et al., 1973). These inorganic radical anions show a lower reactivity than $\bullet\text{OH}$, so that they do not play a role in the decolourisation of RB 19.



With further increases in pH, to pH 11, there is a continuous increase in the efficiency of the dye decolourisation process (Fig. 4). It is known that increasing the pH of the solution increases the concentration of HO_2^- , the peroxide conjugate base (Reaction (8)) (Aleboye et al., 2005; Xu et al., 2009). HO_2^- absorbs the radiation at 254 nm more intensely than the peroxide, which should lead to an increase in the concentration of $\bullet\text{OH}$ radicals (Reaction (9)) (Aleboye et al., 2005; Lergini et al., 1993; Beltran et al., 1997).



But HO_2^- , the conjugate anion of H_2O_2 , reacts with a non-dissociated molecule of H_2O_2 according to Reaction (10), which leads to oxygen (O_2) and water, instead of producing hydroxyl radicals under UV radiation (Reaction (9)). Therefore, the instantaneous concentration of $\bullet\text{OH}$ is lower than expected.



Additionally, at high pH values deprotonation of the RB 19 molecule probably took place, which was confirmed in a study of another anthraquinone dye with a similar structure (Epolito et al., 2005). These structural changes could make the RB 19

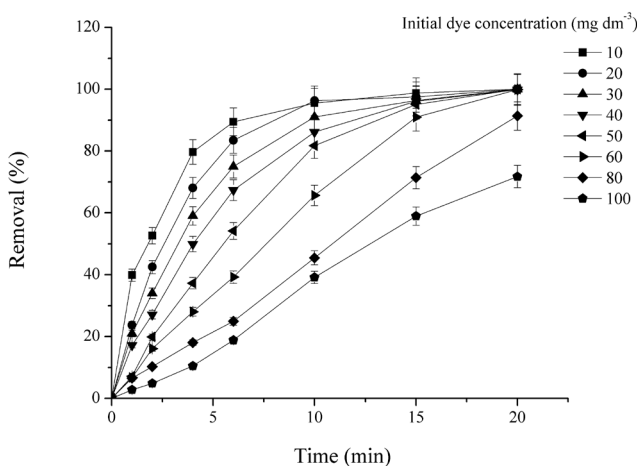


Figure 6

Effect of initial dye concentration on removal of RB 19. $[\text{H}_2\text{O}_2]_0 = 25 \text{ mmol}\cdot\text{L}^{-1}$, initial pH was 7, UV radiation intensity was $1950 \mu\text{W}\cdot\text{cm}^{-2}$, temperature was $25.0 \pm 0.5^\circ\text{C}$.

dye molecule especially vulnerable to $\bullet\text{OH}$ radical attack, leading to an increase in decolourisation rate.

Effect of initial dye concentration

The effect of initial dye concentration on decolourisation by the UV/ H_2O_2 process is shown in Fig. 6. It was found that by increasing the initial dye concentration from 10 to 100 $\text{mmol}\cdot\text{L}^{-1}$ decolourisation decreased ($R^2 = 0.986 - 0.999$). After 10 min of treatment, samples with lower initial concentrations were completely decolourised. The decrease in decolourisation efficiency with increase in dye initial concentration can be explained by the internal filter effect (Ghodbane et al., 2010; Elmorsi et al., 2010). An increase in dye concentration induces a rise in internal optical density and the solution becomes more and more impermeable to UV irradiation. In this way, H_2O_2 can only be irradiated by a small portion of UV light to form fewer free radicals and colour removal decreases (Elmorsi et al., 2010; Ghodbane et al., 2010; Muruganandham et al., 2004; Aleboye et al., 2005; Behnajady et al., 2004; Galindo et al., 1998).

Effect of initial H_2O_2 concentration

Hydrogen peroxide concentration is an important parameter for the degradation of dye by the UV/ H_2O_2 process. The effect of initial peroxide concentration on decolourisation of RB 19 dye has been studied at an initial H_2O_2 concentration ranging from 10 to 100 $\text{mmol}\cdot\text{L}^{-1}$. Results show that increasing H_2O_2 concentration increased dye removal, until the concentration of peroxide reaches approximately 30 $\text{mmol}\cdot\text{L}^{-1}$ (Fig. 7). In this range, the apparent pseudo-first rate constant increases from 0.083 min^{-1} to 0.120 min^{-1} . At H_2O_2 concentrations above 30 $\text{mmol}\cdot\text{L}^{-1}$ the process rate decreases. At low concentrations of H_2O_2 , $\bullet\text{OH}$ radical concentration is proportionally low, which results in a low decolourisation rate. In all experiments, the values of R^2 were higher than 0.98.

By increasing the peroxide concentration more and more hydroxyl radicals are generated. The $\bullet\text{OH}$ free radicals produced upon photolysis of H_2O_2 can react with dye molecules, but also with an excess of H_2O_2 . Excess of hydrogen peroxide and high $\bullet\text{OH}$ radical concentration results in competitive

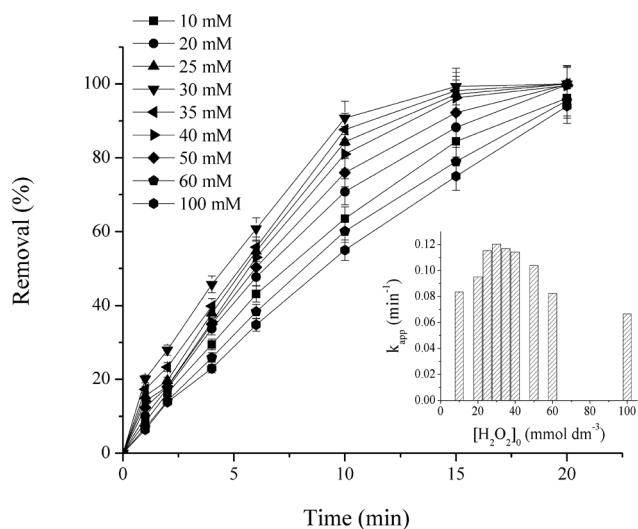


Figure 7

Effect of initial concentration of peroxide on removal of RB 19. $[RB19]_0 = 50 \text{ mg}\cdot\text{L}^{-1}$, initial pH = 7, UV radiation intensity was $1950 \mu\text{W}\cdot\text{cm}^{-2}$, temperature was $25.0 \pm 0.5^\circ\text{C}$. Inset shows the relation between pseudo-first order rate constants and initial concentration of peroxide.

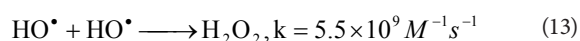
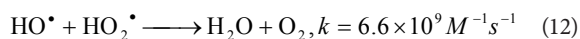
reactions, producing an inhibitory effect on decolourisation (Zollinger et al., 2003; Muruganandham et al., 2004; Aleboeyh et al., 2005; Rezaee et al., 2008).

Other authors have produced similar results in their investigation of this dye. Rezaee et al. (2008) and Guimaraes et al. (2012) also observed high decolourisation of RB 19 solution by the UV/ H_2O_2 process; using H_2O_2 and a low-pressure mercury UV-C lamp, the solution was completely decolourised in less than 30 min.

With a further increase in initial concentration of peroxide from 30 to $100 \text{ mmol}\cdot\text{L}^{-1}$, the rate of decolourisation is reduced and k_{app} values decreased, almost by half, from 0.120 min^{-1} to 0.066 min^{-1} . When the initial peroxide concentration is very high, generated $\bullet\text{OH}$ are mostly reacting with the excess of peroxide and produce $\text{HO}_2\bullet$ radicals, according to Reaction (11) (Aleboeyh et al., 2005; Daneshvar et al., 2005). It is clear that $\text{HO}_2\bullet$ radicals are less reactive than $\bullet\text{OH}$ radicals and the decolourisation rate decreases (Daneshvar et al., 2005).



Generated $\bullet\text{OH}$ radicals can also react with $\text{HO}_2\bullet$ and produce water and dioxygen (Reaction (12)) or dimerize to H_2O_2 (Reaction (13)) (Aleboeyh et al., 2005; Daneshvar et al., 2005):



Therefore, the optimum value of H_2O_2 concentration for the maximum decolourisation rate for RB 19 was approximately $30 \text{ mmol}\cdot\text{L}^{-1}$.

Effect of UV radiation intensity

With increasing UV radiation intensity, the efficiency of dye decolourisation increases considerably. Based on the results obtained (Fig. 8), it can be concluded that the decolourisation

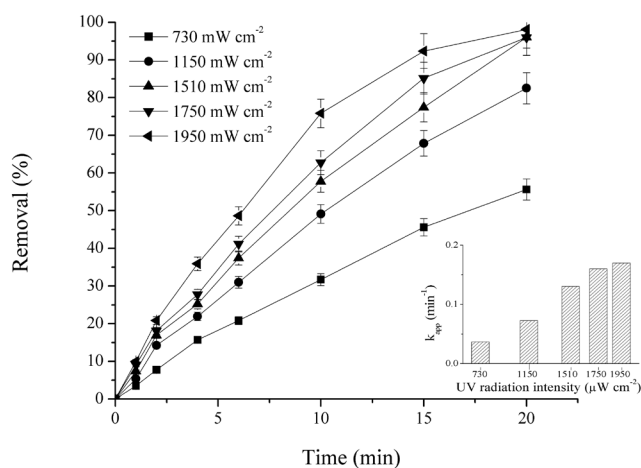


Figure 8

Effect of radiation intensity on removal of RB 19. $[RB19]_0 = 50 \text{ mg}\cdot\text{L}^{-1}$, $[\text{H}_2\text{O}_2]_0 = 25 \text{ mmol}\cdot\text{L}^{-1}$, initial pH = 7, temperature was $25.0 \pm 0.5^\circ\text{C}$. Inset shows the relation between pseudo-first order rate constants and radiation intensity.

rate constant of the dye increases with the increase in radiation intensity from $730 \mu\text{W}\cdot\text{cm}^{-2}$ to $1950 \mu\text{W}\cdot\text{cm}^{-2}$. The smallest increase in process efficiency took place from $1750 \mu\text{W}\cdot\text{cm}^{-2}$ to $1950 \mu\text{W}\cdot\text{cm}^{-2}$; from this it follows that the back lamps in the photoreactor contribute least to dye decolourisation. The results also show that the UV intensity tested in the study lies in the linear range and that all photons produced are effectively used (Fig. 8). R^2 values were from 0.995 to 0.998.

The results of this investigation are consistent with previous studies which generally observed an increase in decolourisation rate with increasing UV intensity (Mills et al., 1993; Lea et al., 1998). This is a consequence of a higher quantity of generated $\bullet\text{OH}$ radicals, which make the oxidative degradation of anthraquinone dye more efficient.

Effect of inorganic ions

It is well known in the textile industry that in order to accelerate or increase the fixation of dyes onto the fibres, it is necessary to use a high electrolyte concentration in the dye bath to decrease the negatively-charged barrier between the cellulose and anionic dyes (Carneiro et al., 2004; Kamyli et al., 2004). We examined the effects of several types of inorganic ions (Cl^- , SO_4^{2-} , NO_3^- , H_2PO_4^-) common in synthetic dye-containing effluent on the photodecolourisation of dyes under UV irradiation. Experiments were done at three different concentrations of inorganic ions: 10, 100 and $1000 \text{ mmol}\cdot\text{L}^{-1}$.

The 20-min decolourisation and the reduction in decolourisation efficiency when adding inorganic anions to RB 19 solutions are shown in Table 3. The degree of inhibition of the process did not increase linearly with increasing inorganic ion concentrations. Furthermore, the overall inhibition is not too extensive despite the fact that high concentrations of inorganic anions are present in solution. This confirms that the UV/ H_2O_2 process can be successfully applied for decolourisation of real textile wastewater which commonly contains high concentrations of inorganic anions.

It can be seen that the 20-min decolourisation efficiency was adversely affected and decreased as the inorganic ion concentrations increased from 10 to $1000 \text{ mmol}\cdot\text{L}^{-1}$ (Fig. 9).

Anion / C _{salt}		10 mmol·L ⁻¹	100 mmol·L ⁻¹	1 000 mmol·L ⁻¹
No salt	Total decolourisation (%)	100	100	100
NO ₃ ⁻	Total decolourisation (%)	81.88	73.62	73.62
	Reduction in decolourisation efficiency (%)	-18.12	-26.38	-26.38
Cl ⁻	Total decolourisation (%)	91.27	86.52	79.07
	Reduction in decolourisation efficiency (%)	-8.73	-13.48	-20.92
SO ₄ ²⁻	Total decolourisation (%)	89.45	81.01	72.00
	Reduction in decolourisation efficiency (%)	-10.55	-18.85	-28.00
H ₂ PO ₄ ⁻	Total decolourisation (%)	84.15	75.89	53.13
	Reduction in decolourisation efficiency (%)	-15.84	-24.10	-46.87

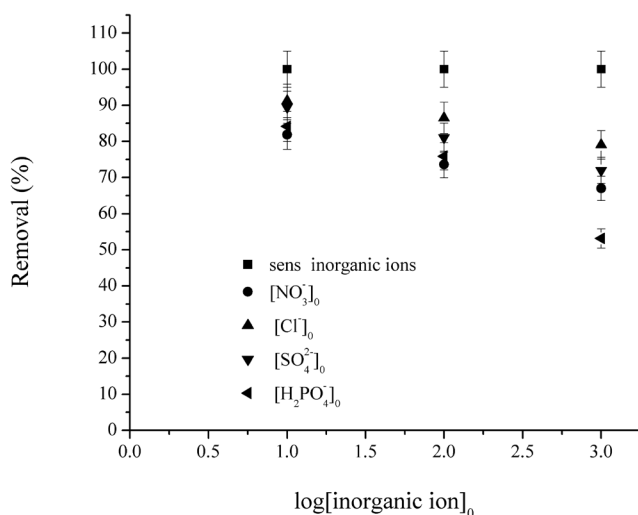
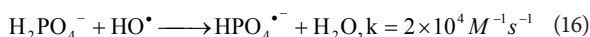
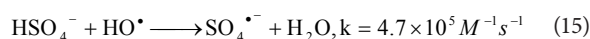
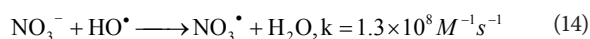
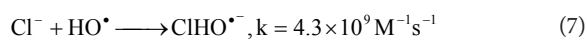


Figure 9

Effect of initial inorganic ion concentrations on removal of RB 19. $[RB19]_0 = 50 \text{ mg}\cdot\text{L}^{-1}$, $[H_2O_2]_0 = 25 \text{ mmol}\cdot\text{L}^{-1}$, UV radiation intensity was $1950 \mu\text{W}\cdot\text{cm}^{-2}$, temperature was $25.0 \pm 0.5^\circ\text{C}$.

At 10 mmol·L⁻¹ and 100 mmol·L⁻¹ the order of inhibition measured was the following: NO₃⁻ > H₂PO₄⁻ > SO₄²⁻ > Cl⁻, while at the higher concentration of 1 000 mmol·L⁻¹, the order of inhibition measured was: H₂PO₄⁻ > NO₃⁻ > SO₄²⁻ > Cl⁻ ($R^2 = 0.964 - 0.999$).

The inhibiting effect of inorganic ions can be explained by the fact that these anions act as •OH radical scavengers, which protect a dye molecule from oxidation (Galindo et al., 2001; Liao et al., 2001). These anions are able to react with hydroxyl radicals leading to inorganic radical ions which show a much lower reactivity than •OH, so that they do not play a role in dye decolourisation. There is also competition between the dye and anions with respect to •OH.



Jaysona et al. (1973) reported that the rate constant for the interaction between •OH radicals and Cl⁻ anions is $k = 4.3 \times 10^9 \text{ M}^{-1}\text{s}^{-1}$ (Reaction (7)). Kastruma et al. (1991) investigated the

reactivity of NO₃⁻ radicals and got the value for rate constant $1.3 \times 10^8 \text{ M}^{-1}\text{s}^{-1}$ for reaction of •OH radical with NO₃⁻ (Reaction (14)). Results of Jiang et al. (1992) and Maruthamuthu et al. (1978), studies showed that HSO₄²⁻ and H₂PO₄⁻ anions react with •OH radical with lower rate ($k = 4.7 \times 10^5 \text{ M}^{-1}\text{s}^{-1}$ and $k = 2 \times 10^4 \text{ M}^{-1}\text{s}^{-1}$, respectively) than NO₃⁻ (Reactions (15) and (16)). Therefore, the obtained scavenging effect of used anions in this study is not in agreement with the values of the rate constants given in the mentioned literature.

CONCLUSION

The results of the present work showed that the UV/H₂O₂ process can be applied as an effective technology for the removal of Reactive Blue 19 from natural and waste waters. Complete decolourisation was achieved after less than 15 min. It was found that with increasing solution pH decolourisation rate increases. The decolourisation of dye decreases by increasing the initial dye concentration from 10 to 100 mmol·L⁻¹. As the initial concentration of H₂O₂ increased from 10 to 30 mmol·L⁻¹, the decolourisation rate constant increased from 0.083 min⁻¹ to 0.120 min⁻¹, while at concentrations above this the process rate decreased. Increasing UV radiation intensity linearly increases the efficiency of dye photodecolourisation. The addition of Cl⁻, SO₄²⁻, NO₃⁻ or H₂PO₄⁻ to the dye solutions examined generally had an adverse effect on the decolourisation rates, but to a varying degree depending on the ion used. The results showed that the degree of inhibition of the process did not increase linearly with an increase in inorganic ion concentration.

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