



# Evaluation of the batch press as a laboratory tool to simulate medium-pressure roller crushers

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## Synopsis

In this study the applicability of a batch press to predict the energy consumption and particle size distributions for medium-pressure roller presses was investigated. The relationships between energy consumption, feed size and product size are discussed with reference to Hukki's interpretation of Bond's and Rittinger's laws, as well as the particle size parameter used. It was found that the comminution laws have limited utility for the characterization of the performance of the medium-pressure roller crushers or the batch press used, and also depend on the particle size distribution indicator used. It was also found that the batch press is not a suitable simulator for medium-pressure roller mills as it was not able to predict the energy requirements, or to predict the size distributions that would be obtained for the ores evaluated.

## Keywords

batch press, roller crushers, comminution, crushing, simulation.

## Introduction

Comminution of ore particles is typically achieved by the application of a mechanical force to a single particle, or a bed of particles, such that the fracture stress of the material somewhere in the particle is exceeded, with resultant fracture and the production of daughter particles. Considering that energy will be required to generate the required stresses in the particles and for the creation of the new surfaces during the fracturing process, it is reasonable to expect that there will be some relationship between the energy consumed by the comminution device and the degree of reduction in particle size achieved. This is indeed the basic idea behind the so-called laws of comminution, as will be discussed later. Considering also that the efficiency of the energy utilization, as well as the size distribution obtained, will probably be dependent on the mode of comminution, i.e. abrasion, impact, or shear, as well as the specific comminution device, it makes good sense to maintain similarity as far as possible when attempting to scale processes. The prediction of the performance of roller crushers poses a problem in that the traditional

approaches, e.g. the Bond work index, would probably not be appropriate, being based on the comminution behaviour of an ore in relatively small ball and rod mills, for which the mechanism and mode of breakage is likely to be quite different from that of the bed of particles that is compacted and sheared in medium- and high-pressure roller crushers, i.e. interparticle crushing. In this work the applicability of the Bond-type approach for predicting the performance of roller crushers is evaluated using a batch press to compress a bed of ore particles. To put this in perspective, the use of roller crushers and the use of the energy approach to predict their behaviour is briefly reviewed.

Austin (1964) proposed that for significant reductions in size, the energy required to mill material is inversely related to the particle size of the product, i.e.

$$\text{Energy} \propto (P_{80})^{-n} \quad [1]$$

where

Energy = energy required for the comminution process

$P_{80}$  = particle size at which 80% of the material will pass when screened

$n$  = exponent characteristic of the comminution device, product size range, and material.

The  $P_{80}$  parameter is extensively used in the design of ball and rod mill circuits and was well researched by Bond for the design of mills by Allis Minerals (Bond 1952). Hukki (1975) investigated the comminution of calcite and

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found that the energy consumption per ton was, as expected, a function of product particle size ( $P_{80}$ ), but also that the value of  $n$  increased significantly at smaller particle sizes, as indicated in Figure 1.

The energy vs. particle size relationship is normally divided into three regions. Above 10 000  $\mu\text{m}$ , or 10 mm, the energy consumption is independent of size; between 10 000 and 100  $\mu\text{m}$  the exponent approximates  $-0.5$ ; and below 100  $\mu\text{m}$  it approximates  $-1$ . The three regions as indicated define the applicability of the so-called comminution laws. The region above 10 mm approximates Kick's law, which states that the energy needed to crush a piece of rock is a function of the flaws present in the particle and thus proportional to the volume of the rock, i.e.

$$\text{Energy} \propto \text{volume} \quad [2]$$

It follows that the energy per unit mass is thus a constant, assuming uniform density, and thus independent of particle size in this particle size range. Bond (1952) found that, for the size ranges typical of ball mills, the energy per unit mass is inversely related to the product size for a constant feed size, i.e.

$$\text{Energy} \propto (P_{80})^{-0.5} \quad [3]$$

or more specifically:

$$\text{Energy} = 10W_i (1/(P_{80})^{0.5} - 1/(F_{80})^{0.5}) \quad [4]$$

where:

$W_i$  = Bond work index (kWh/t)

$P_{80}$  = 80% passing size of the feed ( $\mu\text{m}$ )

$F_{80}$  = 80% passing size of the product ( $\mu\text{m}$ ).

For fine product sizes, i.e. below 100  $\mu\text{m}$ , the energy required to crush a single particle increases exponentially. In this size range the energy required is inversely related to the product size (Austin, 1964):

$$\text{Energy} = kW_i (1/P_{80} - 1/F_{80}) \quad [5]$$

where:

$k$  = constant.

However, there is reason to believe that the size ranges where the various laws apply might differ for different applications. When analysing the energy vs. particle size relationship in Figure 1, it should be noted that Bond's and Rittinger's laws are, respectively, represented by a point on the graph and are only approximated over a wider range of product sizes. One therefore has to rather determine the relationship between energy and product size for the specific

size range of interest. The work done by Hukki and Bond was for single particle crushing conditions, and the applicability of these relationships to the predominantly interparticle crushing mode of roller crushers and a batch press will have to be established. Hukki also questioned the use of the 80% passing size as the descriptor of the particles size in the energy laws. Kapur *et al.* (1990) indeed found that the use of a 50% passing size was more appropriate for describing the relationship between energy and particle size for a high-pressure roller crusher. In this work, the use of both 50% and 80% passing sizes was evaluated using a generalized energy-size parameter relationship:

$$\text{Energy} = (100)^n OW_i (1/(P_x)^n - 1/(F_x)^n) \quad [6]$$

where:

$OW_i$  = operating work index (kWh/ton)

$n$  = particle size exponent

$P_x$  =  $x\%$  passing size of the feed ( $\mu\text{m}$ )

$F_x$  =  $x\%$  passing size of the product ( $\mu\text{m}$ ).

The term operating work index ( $OW_i$ ) is used to indicate a work index determined using the Bond approach, but for other mills.

Interparticle crushing is achieved when a bed of particles, rather than a single particle, is subjected to forces high enough to cause fracture of the particles, as typically occurs with high and medium-pressure roller crushers and to some extent in cone crushers operating under choke-fed conditions. The crushing and milling of material with high- and medium-pressure roller crushers is not new in the world of comminution, but application in the mining industry is still in the early stages. High- and medium-pressure roller crushers have been used for over 30 years for the milling of coking coal for pulverized coal injection in blast furnaces, and for the milling of manganese dioxide, cement, and other fine grinding applications (Eicke, 1979; Schönert, 1988; Schewchten and Milburn, 1990; Mayerhauser, 1990). Limiting over-grinding is a major potential advantage of interparticle crushing (Fandrich *et al.*, 1997). To pursue this benefit a large-scale roller crusher (Loesche) was installed at Foskor in order to limit the over-grinding of the apatite, which causes significant losses during flotation (Van der Linde and Bester, 1998). Interparticle crushers also offer the potential of being more energy efficient than conventional milling (Schönert, 1988, 1991; Mayerhauser, 1990; Norgate and Weller, 1994).

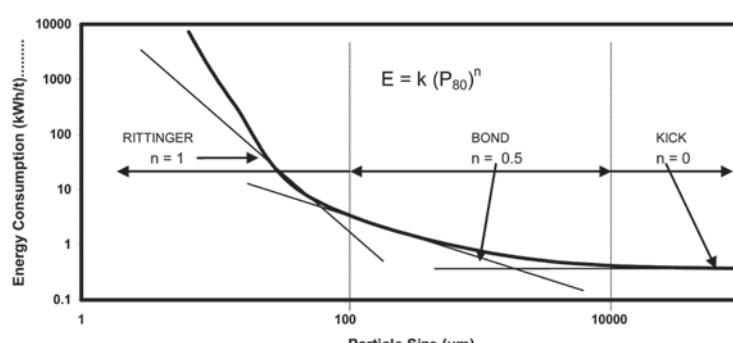


Figure 1—Energy requirements for comminution as determined by Hukki (1975), illustrating the range of applicability of Kick's, Bond's, and Rittinger's laws as indicated by the different applicable values for the exponent in the equation  $E \propto (P_{80})^{-n}$

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A further advantage of roller crushers is the narrower particle size distributions that can be achieved compared to ball and rod milling. In most beneficiation processes too much fine material, normally expressed as  $-38\text{ }\mu\text{m}$  material, leads to a loss of the minerals of interest. Flotation recovery of the fine fractions is lower, magnetic separation of  $-38\text{ }\mu\text{m}$  material is more difficult, and normally too high a slimes content has a negative impact on beneficiation. Viljoen, *et al.* (2001) and Van der Linde and Bester (1998) confirmed this for the flotation of nickel and phosphate ores respectively. In this study it will be shown that the flotation of zinc sulphides could be similarly affected.

The prediction of the performance of roller crushers is problematic in the sense that it is not clear if the existing comminution laws, bench-scale test methods, and particle size descriptions for other crushers also apply to the predominantly interparticle crushing mode of roller crushers. While it is recognized that the Bond-type approach has serious limitations (Napier-Munn *et al.* (1996), the attractiveness of using a simple test such as a batch press, which also fractures particles by interparticle compression in a bed of particles, to predict the performance of roller crushers was worth investigating. This study was focused on the evaluation of a batch press as a small-scale bench test to predict the performance of high- and medium-pressure roller crushers, such as the Horomill pilot unit at FCB in Lille, France and the Loesche pilot mill at AARL in Johannesburg, South Africa.

## Experimental set-up

A pilot plant Horomill, a pilot plant Loesche mill, and a batch press were used for the experiments.

Four ore types were tested:

- A mixed sulfide ore from the Rosh Pinah mine. This is an ore of medium hardness that typically has to be crushed to between  $150\text{ }\mu\text{m}$  and  $50\text{ }\mu\text{m}$ , as the liberation size of the various minerals varies from 106 to  $75\text{ }\mu\text{m}$
- Titanium slag, which is very soft and which should be crushed to top size of  $850\text{ }\mu\text{m}$  with the specific requirement that the  $-106\text{ }\mu\text{m}$  fraction must be minimized
- Apatite ore from Foskor. This is a coarse-grained ore of medium hardness for which overgrinding should be avoided
- Banded ironstone with a liberation size of less than  $100\text{ }\mu\text{m}$ .

## Batch press

The batch press consisted of:

- A cylinder with inside dimensions of 150 mm deep by 140 mm diameter as shown in Figure 2
- A piston with an outside diameter of 138 mm and a height of 200 mm
- A hydraulic press fitted with a load cell and displacement gauge and a personal computer to record the displacement vs. force characteristics of the particle bed. The bed of ore was compressed to a maximum applied pressure.

The tests were done as follows:

- The cylinder was filled with a certain amount of material, mostly 1 kg, leveled using a spatula, and then pressed to the desired pressure. Care was taken not to handle the material extensively or vibrate it, as this caused segregation of the material
- The material was removed, screened, and the mass of the coarse and fine fractions recorded. Fresh feed was added to the coarse fraction to keep the amount of ore in the cylinder at 1 kg, and homogenized by mixing in a bowl with a spatula, taking care to limit the segregation of the material
- The whole sequence was repeated until the mass of the fine fraction remained constant. Five to eight repetitions were normally necessary to achieve this.

## Pilot Horomill tests

The Horomill used in this study consisted of a shell of 0.8 m diameter by 1 m long. Inside the mill a roller is installed, onto which pressure is applied by a set of hydraulic cylinders. The cylinder is driven by an electric motor and gearbox. Material is fed into the feed end, pressed between the roller and shell, and as the bed is compressed to a cake, loosened and moved longitudinally by a set of scrapers inside the mill before being pressed again. This technique enables the mill to press the material three to five times before it exits the mill. The material was fed to the Horomill at feed rates that varied between 1.97 and 3.71 dry tons per hour at a top size of 30 mm and an 80% passing size of 16 mm. Pressures varied between 25 and 30 bar hydraulic pressure which induced a

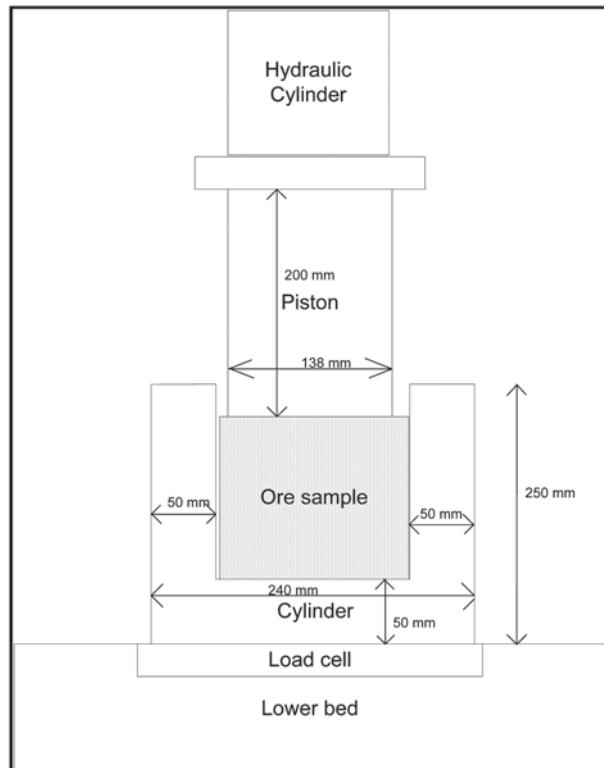


Figure 2—Schematic representation of the batch press. A piston is used to compress the ore sample in the cylinder

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pressure of approximately 30 MPa on the bed of particles. Further detail of this test is given in the report by FCB on the project (Evrard and Cordonnier, 1995).

## Pilot Loesche mill at Anglo American Research Laboratories (AARL)

The set-up at AARL was as follows for the Rosh Pinah and iron ore tests.

- The mill consisted of two 200 mm diameter rollers applying pressure onto a 320 mm diameter table
- The product was swept from the table by an air stream and transported through the internal classifier to a cyclone and baghouse. The oversize joined the feed on the table
- The total energy consumption used during each test was measured by a torque converter installed on the drive shaft of the mill
- For the milling of the titanium slag, an 850  $\mu\text{m}$  aperture external screen was installed and the oversize was added to the feed
- The feed rate to the mill varied between 0.22 to 0.34 dry tons per hour for the Rosh Pinah ore, with top sizes between 3 and 10 mm; 0.3 t/h for the slag, with a top size of 5 mm; and 0.3 t/h for the banded ironstone, with top sizes between 3 and 5 mm.

## Results and discussion

### Comparison between the energy consumption of the batch and pilot mills

#### Foskor ore

The operating work index and the energy consumption needed to crush Foskor ore from a top size of 30 mm to product sizes smaller than 500  $\mu\text{m}$  in the Horomill and from 10 mm to smaller than 500  $\mu\text{m}$  in the batch press as a function of the product size, characterized in terms of the 80% and 50% mass passing sizes, are shown in Figures 3 and 4 respectively. The results obtained for the milling of Foskor ore in a pilot plant ball mill at FCB by Evrard and Cordonnier (1995) are shown in Figure 5. The generalized energy vs. particle size relationships indicated were fitted to the data and are indicated on the graphs as lines. The results from these tests are summarized in Table I.

It follows from the results that the energy-size relationship is not independent of the passing size used, with significantly different values obtained for both the operating work index and the exponent  $n$  for the 50 and 80% passing sizes. It is also notable that the values for  $n$  vary from the expected 0.5 or 1 of the Bond or Rittinger laws. Surprisingly, the value of 1 for the ball mill is significantly different from

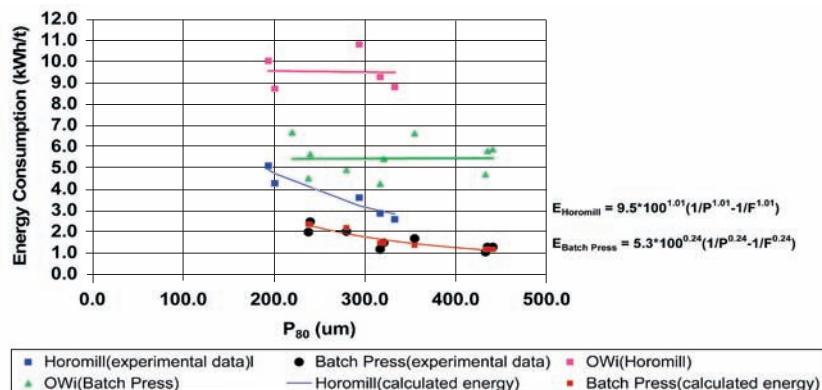


Figure 3—Energy consumption and operating work index plotted as a function of the 80% mass passing size obtained with the Horomill and batch press for an apatite ore from Foskor

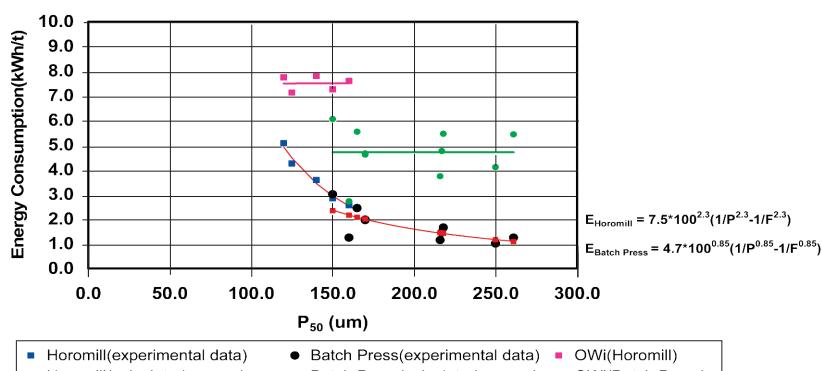


Figure 4—Energy consumption and operating work index plotted as a function of the 50% mass passing size obtained with the Horomill and batch press for an apatite ore from Foskor

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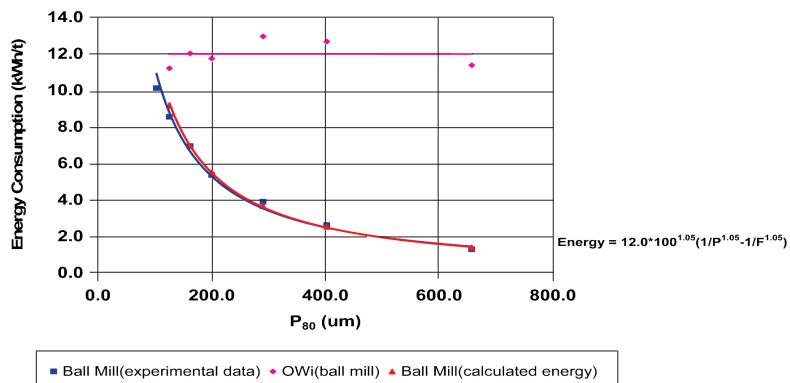


Figure 5 – Energy consumption and operating work index as a function of product size for an apetite ore from Foskor in a pilot ball mill

Table I

Values of operating work indices and coefficient  $n$  for Foskor ore as well as the constants needed to describe the energy-reduction relationship for various comminution devices

Horomill				Batch press				Ball mill						
$F_{80}$ ( $\mu\text{m}$ )	$F_{50}$ ( $\mu\text{m}$ )	$P_{80}$ ( $\mu\text{m}$ )	$P_{50}$ ( $\mu\text{m}$ )	$F_{80}$ ( $\mu\text{m}$ )	$F_{50}$ ( $\mu\text{m}$ )	$P_{80}$ ( $\mu\text{m}$ )	$P_{50}$ ( $\mu\text{m}$ )	$P_{80}$ ( $\mu\text{m}$ )	$OWi$	$n$	$OWi$	$n$	$OWi$	$n$
15300	3000	9.51	1.05	7.5	2.31	2008	620	5.33	0.24	4.7	0.85	12	1.05	

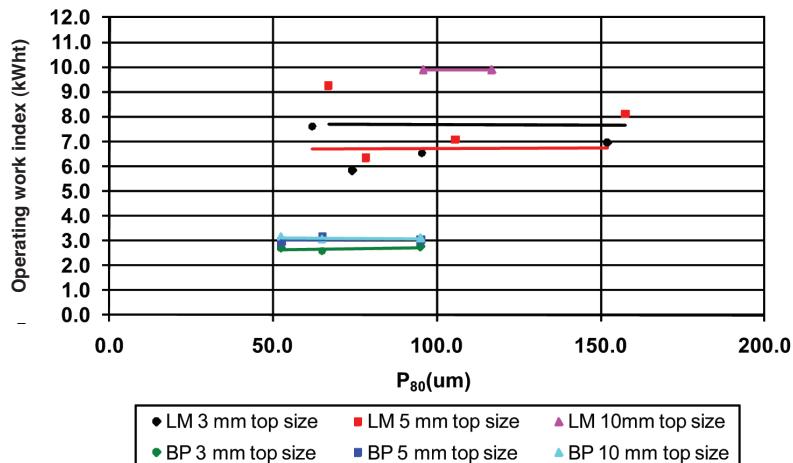


Figure 6—Operating work index plotted as a function of 80% mass passing size for the product of the pilot Loesche mill and batch press on Rosh Pinah ore

the 0.5 expected for the Bond relationship that is typically used for this application. It is also clear that the constants obtained in the batch press experiments differ significantly from those obtained in both the Horomill and the ball mill, indicating that the batch press is probably a poor simulator for these devices.

### *Rosh Pinah ore*

The relationships between the product size and energy consumption for both 80% and 50% passing sizes for the Loesche pilot mill and the batch press for Rosh Pinah ore are

indicated in Figures 6 to 9. The energy consumption and the operating work indices for the ball mill at Rosh Pinah, determined using historical data from 2002, are shown in Figure 10. Only the trend line for the energy consumption is shown in order to keep the graph readable. This graph again emphasizes that, even with ball mills, Bond's law does not apply. The results are summarized in Table II.

It is again clear that the energy-size relationship is not independent of the size descriptor used, i.e.  $P_{80}$  or  $P_{50}$ , with very significant differences in the values of the *OWi*, but smaller differences in the values obtained for  $n$ . However, the fit between the calculated and experimental values is

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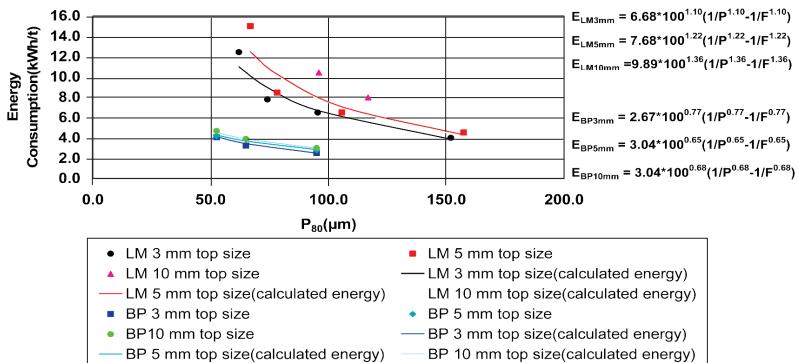


Figure 7—Energy consumption as a function of the 80% mass passing size for the product of the pilot Loesche mill on Rosh Pinah ore

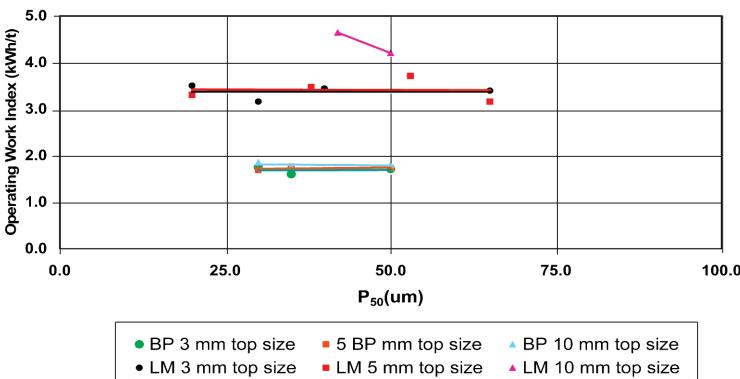


Figure 8—Operating work index plotted as a function of 80% mass passing size for the product of the pilot Loesche mill and batch press for the Rosh Pinah ore

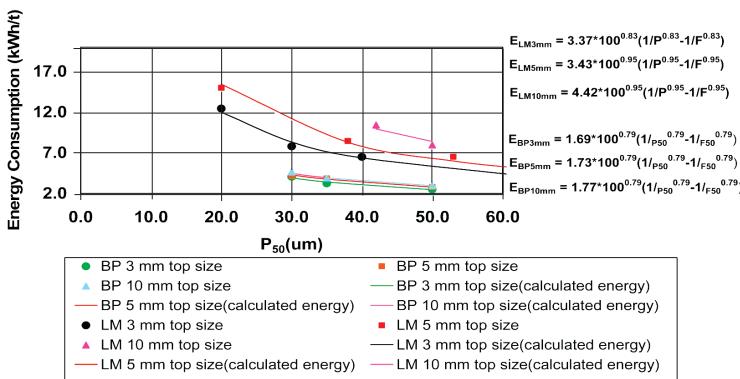


Figure 9—Energy consumption as a function of the 50% mass passing size for the product of the pilot Loesche mill on Rosh Pinah ore

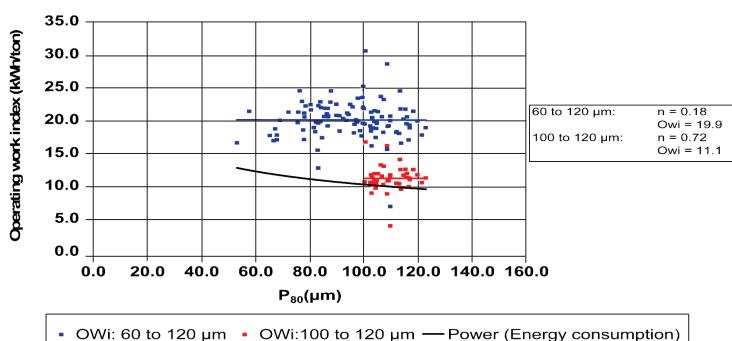


Figure 10—Energy consumption and operating work indices plotted as a function of 80% mass passing size for the product of the Rosh Pinah ball mill. The operating work index is for two different size ranges

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Table II

Values of operating work indices and coefficient  $n$  for the Loesche mill and batch press on Rosh Pinah ore

Top size	Loesche mill						Batch press					
	$F_{80}$ (mm)	$F_{50}$ ( $\mu\text{m}$ )	$P_{80}$ ( $\mu\text{m}$ )		$P_{50}$ ( $\mu\text{m}$ )		$F_{80}$ ( $\mu\text{m}$ )	$F_{50}$ ( $\mu\text{m}$ )	$P_{80}$ ( $\mu\text{m}$ )		$P_{50}$ ( $\mu\text{m}$ )	
			$OWi$	$n$	$OWi$	$n$			$OWi$	$n$	$OWi$	$n$
3 mm	1500	530	6.68	1.10	3.33	0.83	1500	530	2.67	0.77	1.69	0.79
5 mm	3000	1600	7.18	1.22	3.43	0.95	3000	1600	3.04	0.65	1.73	0.80
10 mm	5800	3350	9.89	1.36	4.42	0.95	5800	3350	3.04	0.68	1.71	0.79

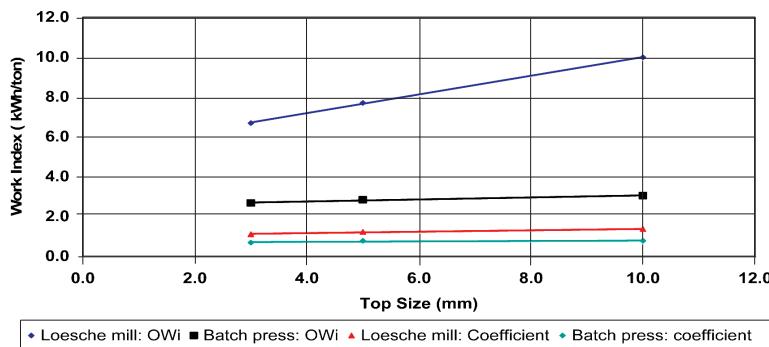


Figure 11—Operating work index and coefficient  $n$ , based on the  $P_{80}$  plotted as a function of top size to compare the pilot Loesche mill with the batch press for the Rosh Pinah ore

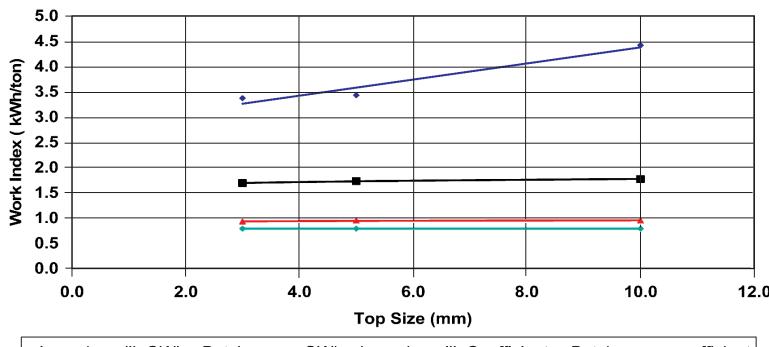


Figure 12—Operating work index and coefficient  $n$ , based on the  $P_{50}$ , plotted as a function of top size to compare the pilot Loesche mill with the batch press for Rosh Pinah ore

reasonable, indicating that the generalized energy-size relationship is valid for this ore and the comminution devices used. The results again indicate that the batch press is not a good simulator for the roller mill, with much lower work indices and significantly different values for  $n$ , especially when using the  $P_{80}$  size descriptor. The influence of the feed size used in the experiments on the work index was also investigated, and the results shown in Figures 11 and 12 indicate that the energy requirements for the roller mill increase with feed top size, while that for the batch press remains constant, over the range investigated. The results for the roller mill are summarized in Table III. Daniel (2001) suggested that the increase in energy may be due to the fact that particles larger than the gap between the rollers may increase the friction on the rollers without actually being nipped and broken, with the effect decreasing as the particle size approaches the gap size. Unfortunately, this could not be

confirmed with the present results, as feed sizes as small as the 2–3 mm gap size on the operating roller mill were not evaluated.

Table III

The influence of the feed size on the energy consumption and operating work indices for the comminution of Rosh Pinah ore in a roller crusher

$F_{80}$ ( $\mu\text{m}$ )	$P_{80}$ ( $\mu\text{m}$ )	Energy consumption (kWh/t)	$OWi: n = 1.1$	$OWi: n = 1.36$
11400	6900	0.44	109.3	281.7
6900	2600	3.104	169.8	354.9
2600	2100	0.211	28.7	52.6

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## Titanium slag

The results of the comminution experiments on the titanium slag are shown in Figures 13 to 16. The values for the  $OW_i$ , as well as the energy-particle size relationship, again differed significantly, depending on whether the  $P_{80}$  or  $P_{50}$  particle size indicator was used. The very low value for the particle size coefficient  $n$  of 0.06 in the energy-particle size relationship for the roller mill is notable, but difficult to explain. The results for the roller mill and the batch press also again differed significantly, indicating that the batch press would not be a good simulator for the roller mill for this ore.

## Banded ironstone

The results of the comminution experiments on the banded

ironstone are shown in Figures 17 to 20. The fitting of the data to obtain the curves shown was problematic in that constant values for the operating work indices could not be obtained unless a very low value of the exponent  $n$  was assumed, which then delivered unrealistically high values for the operating work indices. If the exponent  $n$  was taken to be 0.21, the fit with the data was still not good, but more realistic values for the operating work indices ranging from 9.1 to 15.7 kWh/t were obtained. These values were considered to be reasonable in view of the expected greater energy efficiencies of the roller mill and batch press, as well as the Bond tests values of approximately 20 kWh/t determined earlier by Cook (2003) for this ore. The effect of the top feed size on the  $OW_i$  was not consistent, with little influence noted if the  $P_{80}$  was used but significantly lower

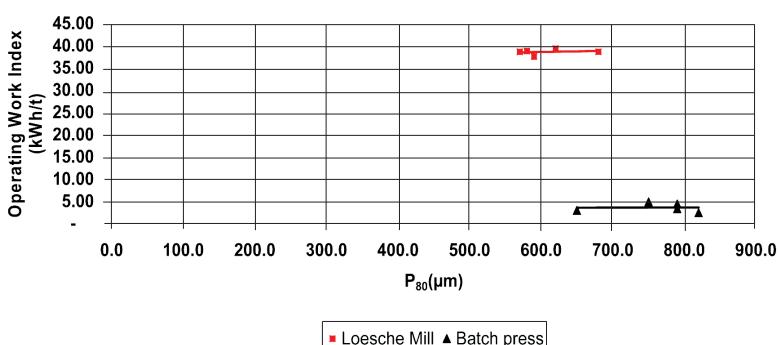


Figure 13—Operating work index as a function of 80% mass passing size for the batch press and the Loesche mill on titanium slag

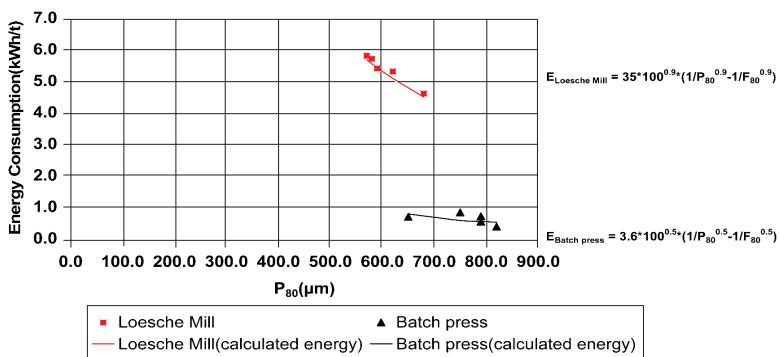


Figure 14—Energy consumption as a function of 80% mass passing size for the batch press and the Loesche mill on titanium slag

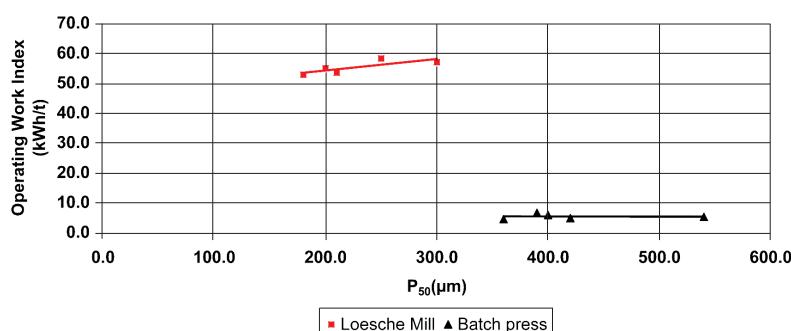


Figure 15—Operating work index as a function of 50% mass passing size for the batch press and the Loesche mill on titanium slag

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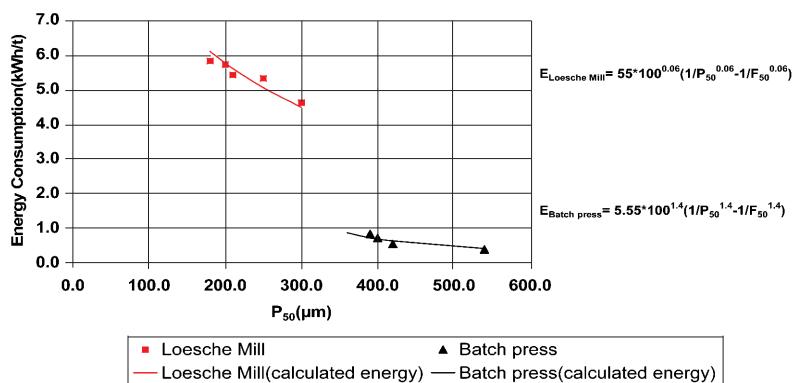


Figure 16—Energy consumption as a function of 50% mass passing size for the batch press and the Loesche mill on titanium slag

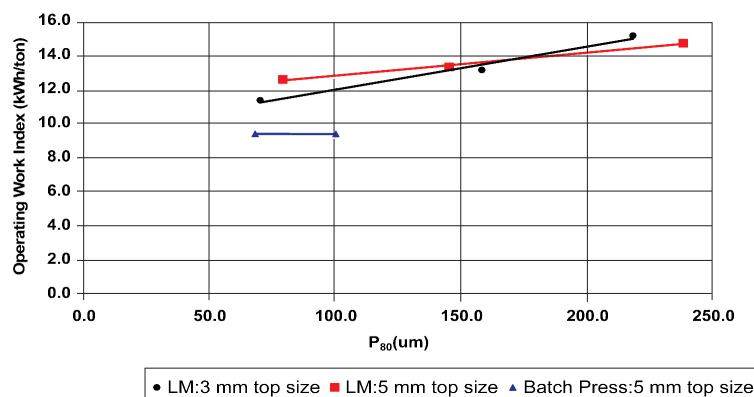


Figure 17—Operating work index plotted as a function of 80% mass passing size obtained with the Loesche mill and the batch for the banded ironstone

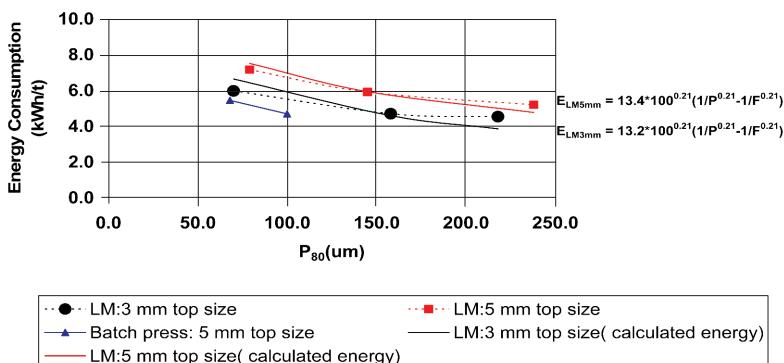


Figure 18—Energy consumption as a function of 80% mass passing size for the Loesche mill and batch press for the banded ironstone

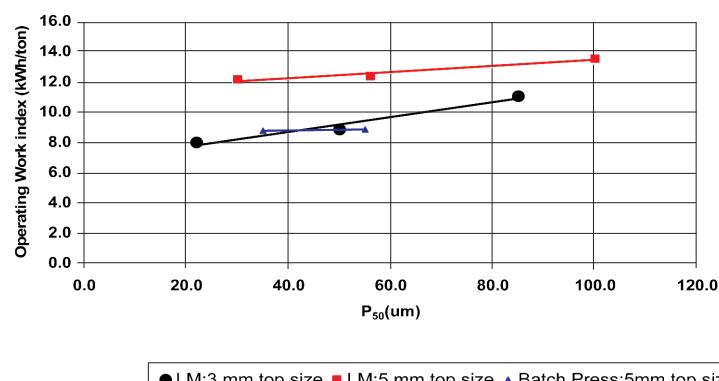


Figure 19—Operating work index plotted as a function of 50% mass passing size for the Loesche mill and batch press for the banded ironstone

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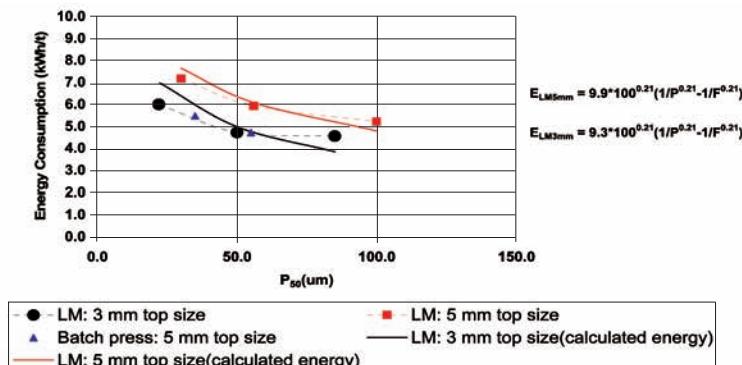


Figure 20—Energy consumption as a function of 50% mass passing size for the Loesche mill and batch press on banded ironstone

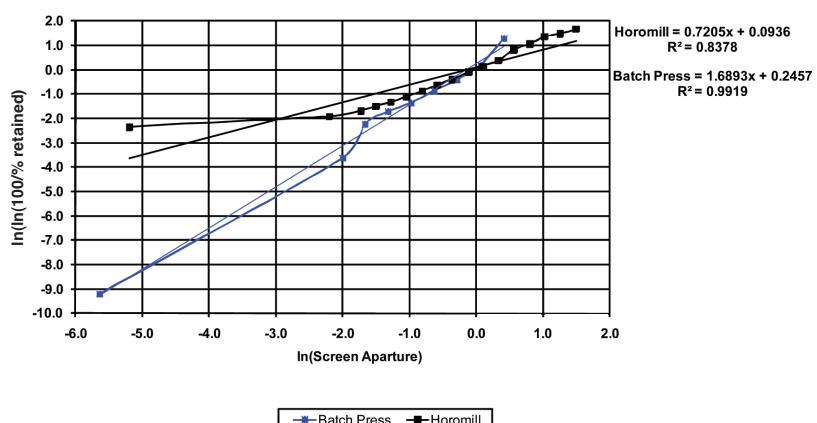


Figure 21—Rosin-Rammler plots of the size distributions obtained with the Horomill and batch press, for the Foskor ore

Table IV

## Operating work indices and coefficients obtained in comminution tests with the Loesche mill and the batch press for the banded ironstone

Values of $OW_i$ and $n$ for banded ironstone					
Top size	$F_{80}$	$OW_i$	$n$	$F_{50}$	$OW_i$
5 mm	3350	13.4	0.21	2300	9.9
3 mm	1750	13.2	0.21	950	9.3
Batch press	3350	9.1	0.21	2300	15.7
					0.18

values if the  $P_{50}$  was used. The similarity between the results obtained with the roller mill and batch press was better for this material, but in view of the problems with the interpretation of the data the batch test cannot be recommended with confidence as a simulator for the roller mill.

## Particle size distributions

The screen analyses of the mill products obtained with the comminution devices for the various ores were plotted as Rosin-Rammler plots, i.e.  $\ln(\ln(100/\% \text{ retained}))$  vs.  $\ln(\text{screen aperture})$ , and are shown in Figures 21 to 26.

Rosin-Rammler plots are useful for simulation studies as the size distributions resulting from ball milling typically give straight line relationships. This was indeed true for most of the tests done, with the notable exceptions of the Foskor ore milled with the Horomill, and for the Rosh Pinah ore milled in the Loesche mill, where in both cases large deviations were notable for the smaller sizes. The simulation of the size distribution of the comminution devices by the batch press was poor, except in the case of the banded ironstone for which the size distributions obtained for the Loesche mill and batch press were comparable.

## Conclusions

The results of this work indicate that:

- The energy-size distribution relationships, e.g. the so-called comminution laws, have limited utility for the characterization of the performance of the roller mills and the batch press for the ores evaluated. The exponent  $n$  required to obtain reasonable fits with the data differed significantly from the 0.5 and 1 used, for the Bond and Rittinger relationships respectively
- The energy-size distribution relationships are dependent on the size distribution parameter chosen with significant differences being obtained depending on whether the 50% or 80% passing size is used
- The constants typically used in the generalized energy

# Evaluation of the batch press as a laboratory tool to simulate medium-pressure roller crushers

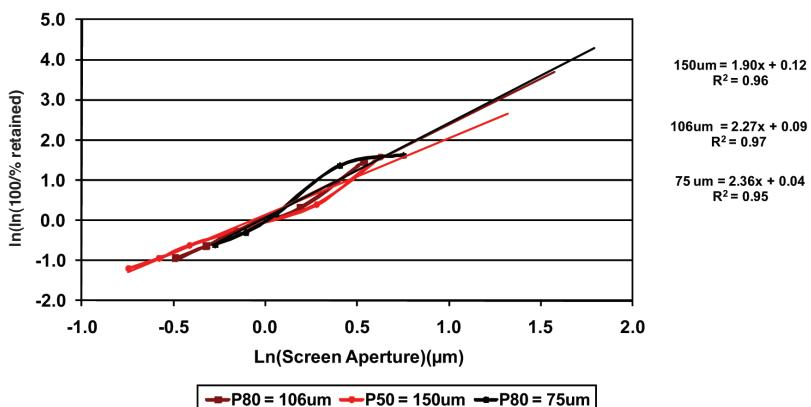


Figure 22—Rosin-Rammler plots of the size distributions obtained with the batch press for the Rosh Pinah ore

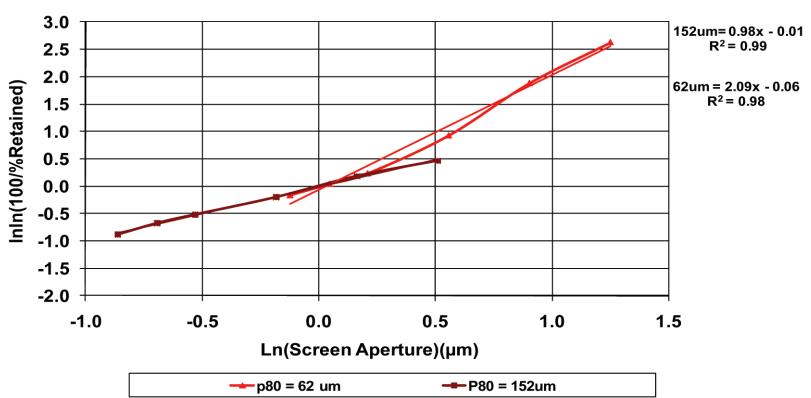


Figure 23—Rosin-Rammler plots of the size distributions obtained with the Loesche mill for the Rosh Pinah ore

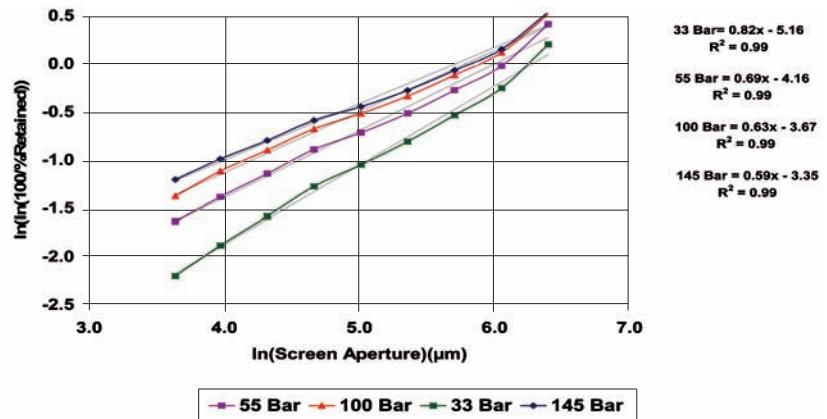


Figure 24—Rosin-Rammler plots of the size distributions obtained with the Loesche mill for the titanium slag. The numbers in the legend indicate the hydraulic pressures at which the mill was set

relationship, i.e. the operating work index ( $OW_i$ ) and the exponent  $n$ , were found to depend on the comminution device and the product size. Analysis of the performance of the industrial-size Rosh Pinah ball mill indicated that the size exponent may significantly differ from the Bond exponent of 0.5 typically assumed for ball mills

► The batch press as operated in the present tests is not a good simulator for roller mills, since it was typically not

possible to meaningfully predict the energy requirements or size distributions of the roller mill products using batch test results

► The Rosin-Rammler size distribution description should be used with caution for roller mills, as significant deviations from the  $\ln(\ln(100\% \text{ Retained}))$  vs.  $\ln(\text{screen aperture size})$  were noted for the Foskor and Rosh Pinah ores, while good fits were obtained for the titanium slag and the banded ironstone.

# Evaluation of the batch press as a laboratory tool to simulate medium-pressure roller crushers

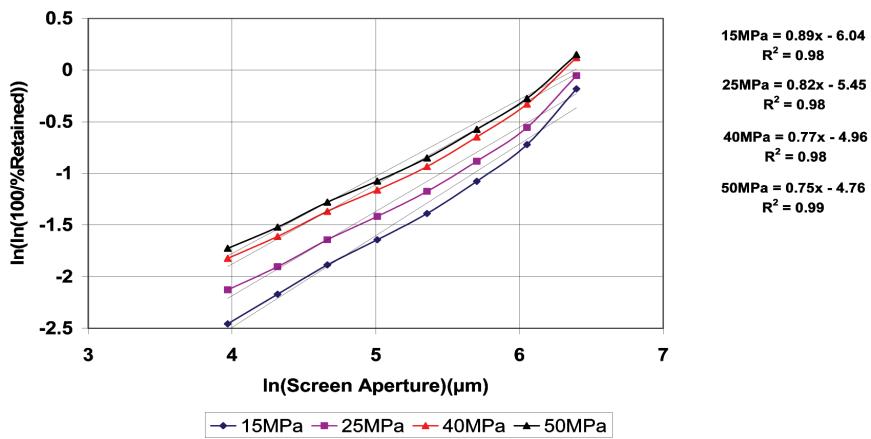


Figure 25—Rosin-Rammler plots of the size distributions obtained with the batch press for the titanium slag. The numbers in the legend indicate the pressures applied to the bed

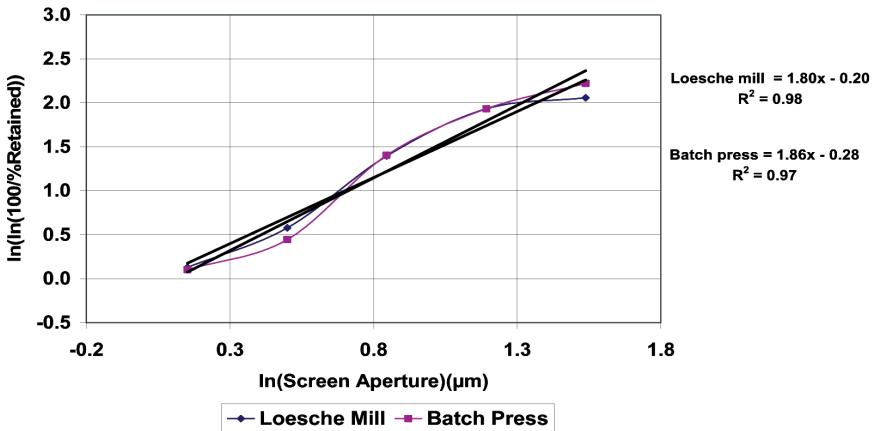


Figure 26—Rosin-Rammler plots of the size distributions obtained with the Loesche mill and the batch press for the banded ironstone

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